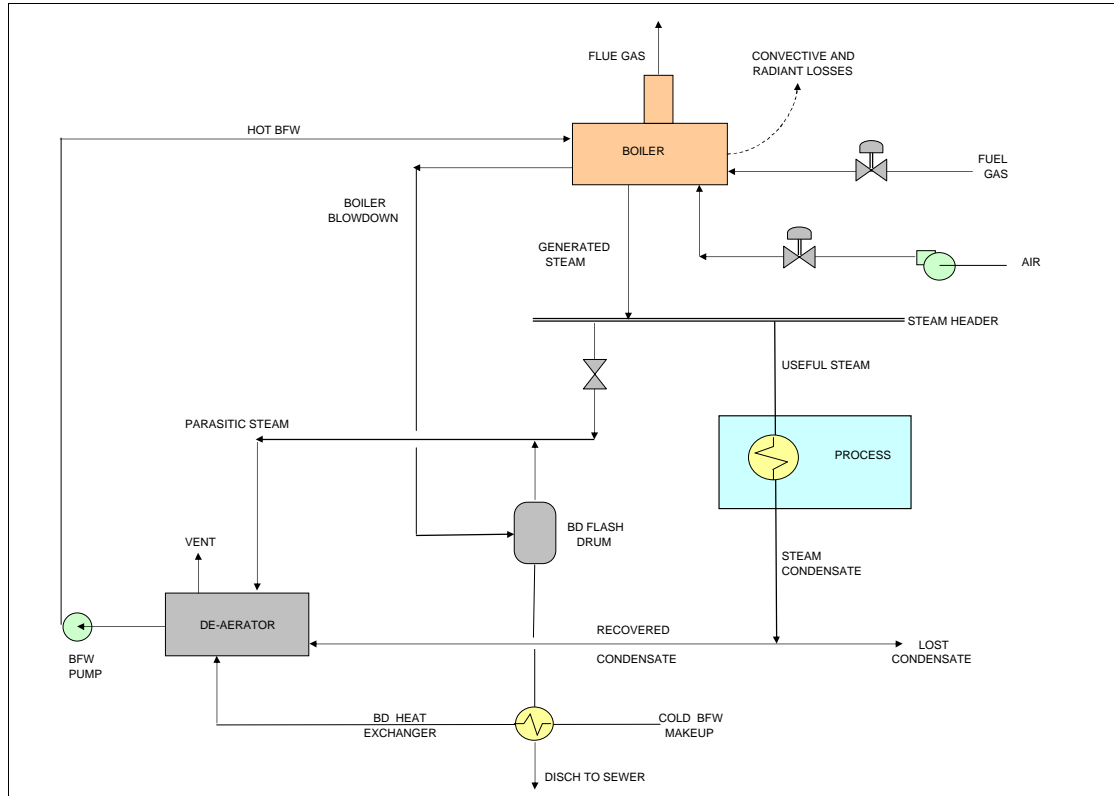


BOILER EFFICIENCY OPTIMIZATION												
PROJECT ID:	US Dept of Energy						EQUIP No:	B-4				
PLANT LOCATION:	Anytown						DATE:	9/10/2007				
SERVICE:	Gas fired boiler (baseload)						ENGR:	J D Kumana				
COLOR CODES:	123	measured value (input)										
	321	iteration parameter										
	456	design paramter (input)										
BASIC DATA												
Fuel =	mixed hydrocarbon gases with composition as below											Stoich oxygen
	MW	C	H	lb/scf	scf/lb	Vol %	lb/h	mol/h	HHV	LHV	oxygen	
									Btu/scf	Btu/scf	mol/h	
Inerts	36	0	0	0.0950	10.5	4.3	1470	40.8	0	0	0	
CO	28.01	1	0	0.0739	13.5	0.2	53	1.9	321	321	2	
H2	2.016	0	2	0.0053	188.0	0.5	10	4.7	324	274	2	
CH4	16.04	1	4	0.0423	23.6	84.5	12874	802.6	1010	911	1605	
C2H6	30.07	2	6	0.0793	12.6	8.0	2285	76.0	1769	1622	266	
C3H8	44.1	3	8	0.1164	8.6	2.0	838	19.0	2516	2318	95	
C4H10	58.12	4	10	0.1534	6.5	0.5	276	4.7	3255	3015	31	
C5H12	72.15	5	12	0.190	5.3	0.0	0	0.0	3978	3682	0	
					20.2	100.0	17806	949.9	1064	963	2001	
HHV reported by Lab Analysis				1060	Btu/scf		37432 Btu/nm3 (HHV)					
Deviation from calculated value =				-0.4	%	OK						
Ambient (basis) temp		80	F				Stm gen rate (trial)	283.9 Klb/h				
Fuel Gas firing rate		6000	scfm (plant data)				Calculated Stm Gen	283.9 Klb/h				
		17806	lb/h				Boiler steam gen capacity	375 Klb/h				
Gas molecular weight		18.7	lb/mole					188 TPH				
Stoichiometric air (dry)		9.96	scf/scf gas				Full-load heat input (fuel)	506 MMBtu/h				
		15.41	lb/lb gas				Boiler operating load	76 %				
Relative Humidity of air		54	%					142 TPH OK				
Water vapor partial press		0.51	psia				Steam pressure	625 psig				
Moisture content		1.92	lb H2O/100 lb dry air					640 psia				
Measured oxygen in FG		3.03	%				Steam sat temp	493 F				
Calc Oxygen in fluegas		3.03	%				Steam superheat	235 F				
Measured CO in flue gas		400	ppm				Steam temp (actual)	728 F				
Excess air		16.0%					Sat steam enthalpy	1201 Btu/lb				
Actual air flow		318.3	Klb/h (dry basis)				Cp of superheated steam	0.6944 Btu/lb-F				
Water vapor in supply air		6.1	Klb/h				Superheated stm enthalpy	1364 Btu/lb				
Air preheating		0	F				BFW flow	285.9 Klb/h				
Air supply temp		80	F				BFW temp	308 F OK				
Flue gas flow (dry)		336.1	Klb/h				BFW enthalpy	278 Btu/lb				
Water of combustion		34.8	Klb/h				Blowdown, % of steam	0.7 %				
Flue gas temp, F		400	F				Blowdown enthalpy	480 Btu/lb				
water vapor enthalpy		1241	Btu/lb									
Combustibles in Flue Gas		600	ppm				Boiler dimensions, ft					
Unburned fuel		0.21	%				Height	60				
							Length	40				
Wall surface material		1	Use 1 for metal, and 2 for brick				Width	25				
Wind velocity		3	ft/sec									
Boiler surface area		7800	ft2 (vertical faces only)				Boiler wall temp	140 F				
Convective Coeff (still air)		0.98	Btu/ft2-h-F				Amb temp in boilerhouse	97 F				
Convective losses		0.5	MMBtu/h				Temp diff vs ambient	43 F				
Estimation of Radiative losses:												
Emissivity of boiler walls:		0.9					Number of Openings in boiler wall	6				
Radiant heat flux		52	Btu/ft2-h				Diameter, or width (if rectangular)	8 inches				
Radiant heat loss (walls)		0.40	MMBtu/h				Approx area of opening/peephole	60 sq in				
Radiant heat loss (holes)		0.61	MMBtu/h				Boiler wall thickness (incl insul)	4 inches				

Radiant heat loss (total)	1.01	MMBtu/h		Radiant loss factor (average)	0.722
				Temp in combustion space	3271 F
(a) Stefan-Boltzmann law:	0.26	% of fuel heat input		Blackbody radiant flux	335204 Btu/ft ² -h
(b) empirical correlation:	0.47	%			
(c) ASME correlation	0.34	% (without ΔT or air velocity corrections)			
	↓				
Radiant heat losses	0.40	% (choose value based on three alternative estimates above)			
HEAT BALANCE					
Heat in fuel (HHV)	383.0			Unburned fuel	0.8
Heat in combustion air	3.7			Radiant loss	1.5
Heat in air moisture	0.1			Convective loss	0.5
Heat in BFW	79.4			Flue gas	75.1 (including water vapor)
Total heat inputs	466.2	MMBtu/h		Blowdown	1.0
				Total heat losses	79.0 MMBtu/h
Heat in steam	387.3	MMBtu/h			
EFFICIENCY CALCULATION (modified ASME method)					
				MMBtu/h	JDK Note
Primary Input (Fuel, HHV)			383.0		ASME method takes credit for heat content of condensed moisture in flue gas as if it were a useful output.
Losses:	Flue gas (sensible)		27.8		Same for boiler blowdown.
	Flue gas (moisture of combustion)		41.5		These are not realistic assumptions.
	Radiation		1.5		
	Convection		0.5		
	Unburned fuel		0.8	Boiler Efficiency =	81.2% by ASME method
	Total		72.2		80.4% by heat balance
Useful Output (net steam vs BFW)			308.7	Optimum air flow =	316 Klb/h
					4124 Kscfh
NOTE: Strictly speaking, the power consumption for BFW pumps, ID/FD fans, etc should also be included as part of the total energy input required to run the boiler. The electric power consumed should be traced back to the point of generation, and the effective heat rate for power gen should be used.					

Developed by: Kumana & Associates
jkumana@aol.com



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